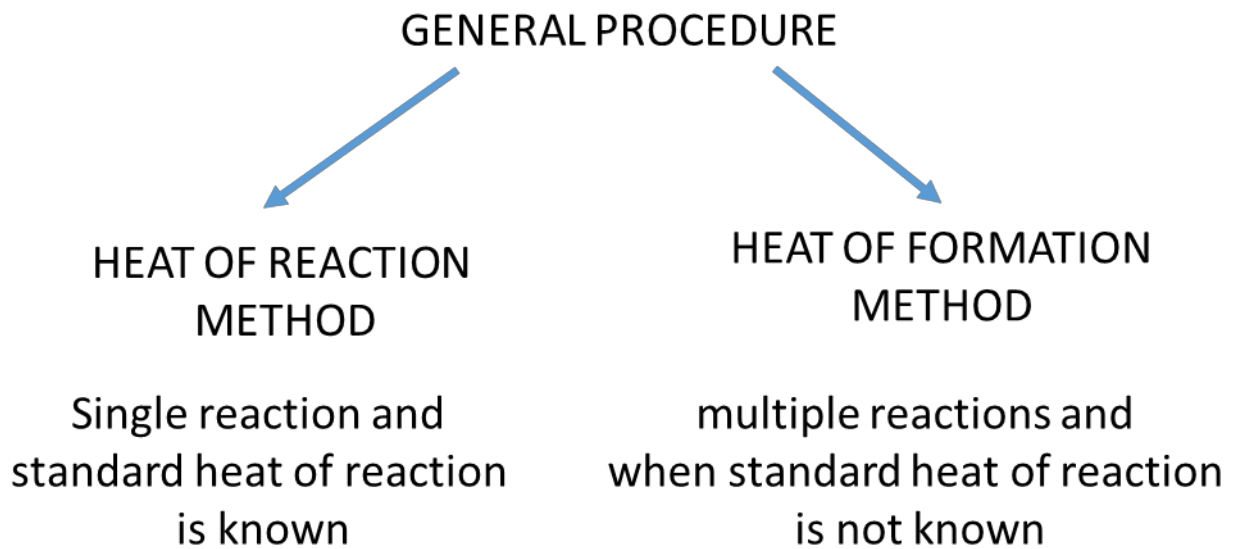


## CEN 205 MASS AND ENERGY BALANCES

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### BALANCES ON REACTIVE PROCESSES:



### HEAT OF REACTION METHOD:

1. Complete all the material balance calculations.
2. Choose the reference states for specific enthalpy calculations. The references are the reactants and products at 25°C and 1 atm in the phases.
3. For a single reaction calculate the extent of reaction

4. Prepare the inlet and outlet enthalpy table.
5. Calculate each unknown enthalpy according to the reference state.
6. Calculate  $\Delta H$  for the reactor.

$$\Delta H = \xi \Delta H_r^o + \sum n_{out} H_{out} - \sum n_{in} H_{in}$$

7. Substitute the calculated value of  $\Delta H$  in the energy balance equation.

$$\Delta H = \sum n_{out} H_{out} - \sum n_{in} H_{in}$$

#### HEAT OF FORMATION METHOD

1. Complete all the material balance calculations.
2. Choose the reference states for specific enthalpy calculations. The references are the elemental species that constitute the reactant and product species ( $C_s$ ,  $O_{2(g)}$ ,  $H_{2(g)}$ ) at  $25^\circ\text{C}$  and 1 atm.
3. Prepare the inlet and outlet enthalpy table.
4. Calculate each unknown enthalpy according to the reference state.
5. Calculate  $\Delta H$  for the reactor.

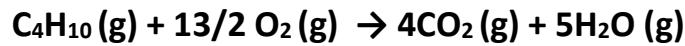
$$\Delta H = \sum n_{out} H_{out} - \sum n_{in} H_{in}$$

6. Substitute the calculated value of  $\Delta H$  in the energy balance equation.

## YOUR TURN

I.

n-Butane (n-C<sub>4</sub>H<sub>10</sub>) at 25 °C is burned with excess air (at 100 °C) in a continuous combustion chamber

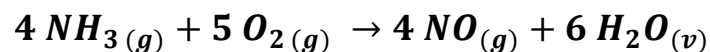


The product gas (at 250°C) contains 0.25 mol% butane, 5.9 mol% oxygen (O<sub>2</sub>), 11.4 mol% carbon dioxide (CO<sub>2</sub>) and the balance nitrogen on dry basis.

- Assume 100 mol of dry product as basis. Draw and label the flow chart.
- Calculate the fractional conversion of n-butane (mol reacted/ mol fed), amount of water (mol H<sub>2</sub>O (g)) leaving the combustion chamber and the amount of excess air.
- Calculate the amount of heat that is transferred to or from the combustion chamber if n-butane enters at 25°C, air enters at 100°C and all the products leave at 250°C.

II.

Ammonia is oxidized in a continuous reactor;



$$\Delta H_{\text{r}}^0 = -904.7 \text{ kJ/mol}$$

The feed stream (containing NH<sub>3</sub> and O<sub>2</sub>) enters at 200°C and the products (O<sub>2</sub>, NO and H<sub>2</sub>O) leave at 1200°C. The mole ratio of NH<sub>3</sub> to O<sub>2</sub> in the feed is 2:3 (NH<sub>3</sub> / O<sub>2</sub> = 2:3). Draw and label the flow chart. Calculate the required heat transfer to or from the reactor.

III.

A superheated gas mixture at 600°C and 1 atm flowing at a rate of 28.5 m<sup>3</sup> (STP)/h is to be cooled to 450°C in an adiabatic spray cooler. The gas mixture contains 17.1 mole % water vapor, H<sub>2</sub>O (v) and has a dry-basis composition of 7.5 mole% CO, 11.5% CO<sub>2</sub>, 1% O<sub>2</sub> and 80 % N<sub>2</sub>. A liquid water at 20°C is sprayed into the hot gas at a rate of m (kg H<sub>2</sub>O (l)/ h). Calculate the liquid water feed rate (m) in kg/h.

