## **CEN 3311 HEAT TRANSFER**

## **UNSTEADY-STATE CONDUCTION CONVECTION BOUNDARY CONDITIONS** (Heat flow with variable surface temperature)

## Semi-infinite solid



•  $T_s \neq T_\infty$ 

• The energy equation for this system (no heat generation, one- dimensional flow, unsteady-state condition)

$$\frac{\partial T}{\partial t} = \propto \frac{\partial^2 T}{\partial x^2} \dots (1)$$

- There is no accumulation of energy at the interface, so the heat flux to the surface equals the flux into the solid.
- Heat convected to surface = heat conducted into surface.

$$hA(T_{\infty} - T)\Big|_{x=0} = -kA\frac{\partial T}{\partial t}\Big|_{x=0}$$
$$x = o T = T_{s}$$

$$hA(T_{\infty} - T) = -kA\frac{\partial T}{\partial t}\Big|_{x=0} \dots \dots \quad (2)$$

• The solution of Eq(1) using Eq(2) as a boundary condition gives:

$$\frac{T - T_a}{T_{\infty} - T_a} = 1 - erfx - \left[exp\left(\frac{hx}{k} + \frac{h^2\alpha t}{k^2}\right)\right]x\left[1 - erf\left(X + \frac{h\sqrt{\alpha t}}{k}\right)\right]$$

Here: 
$$X = \frac{x}{2\sqrt{\propto t}}$$



Figure 4-5 | Temperature distribution in the semi-infinite solid with convection boundary condition.



**Figure 4-7** | (*Continued*). (*b*) expanded scale for 0 < Fo < 4, from Reference 2.

Midplane temperature (To) for an infinie plate of thickness of 2s (scale for 0<Fo>4)



**Figure 4-8** | Axis temperature for an infinite cylinder of radius  $r_0$ : (*a*) full scale.



Credit: Holman (2010) Heat Transfer, 10<sup>th</sup> Ed.







**Figure 4-9** Center temperature for a sphere of radius  $r_0$ : (*a*) full scale.



Credit: Holman (2010) Heat Transfer, 10<sup>th</sup> Ed.





