

**CEN 3313**

**MASS TRANSFER**

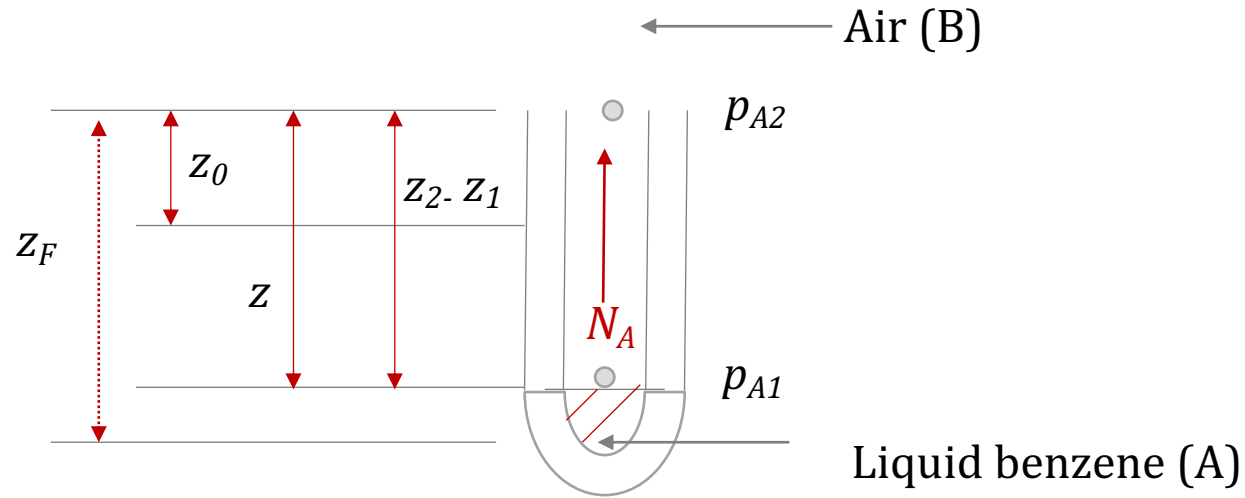
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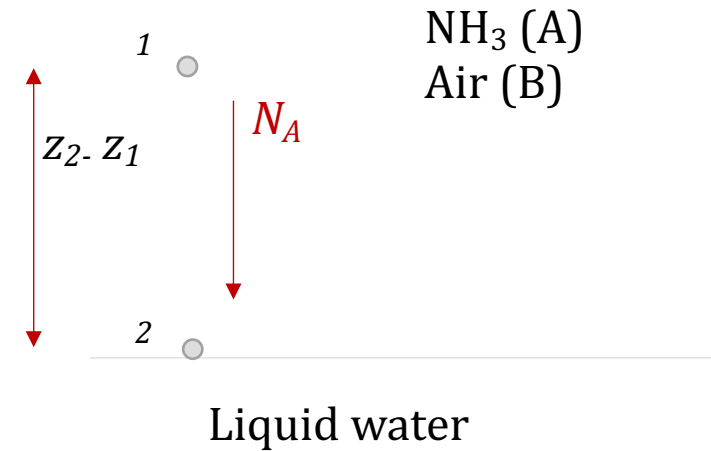
# Molecular Diffusion in Gases- Special Case for A Diffusing Through Stagnant, Nondiffusing B

Impermeable boundary to component B



**Benzene evaporating into air**

**$(N_B = 0)$**



**Ammonia in air being absorbed into water**

**$(N_B=0)$**



# Molecular Diffusion in Gases-

## Special Case for A Diffusing Through Stagnant, Nondiffusing B

$$N_A = -cD_{AB} \frac{d(x_A)}{dz} + \frac{c_A}{c} (N_A + N_B)$$

$N_B = 0$

$$N_A = -cD_{AB} \frac{d(x_A)}{dz} + \left(\frac{c_A}{c}\right) (N_A + 0)$$

$$c = \frac{P}{RT}; \quad p_A = x_A P; \quad \frac{c_A}{c} = \frac{p_A}{P}$$

$$N_A = -\frac{D_{AB}}{RT} \frac{d(p_A)}{dz} + \frac{p_A}{P} N_A$$

$$N_A \left(1 - \frac{p_A}{P}\right) = -\frac{D_{AB}}{RT} \frac{d(p_A)}{dz}$$

Constant  
Pressure

$$N_A = -D_{AB} \frac{P}{RT} \frac{1}{(P - p_A)} \frac{d(p_A)}{dz}$$

$$N_A \int_{z_1}^{z_2} dz = -D_{AB} \frac{P}{RT} \int_{p_{A1}}^{p_{A2}} \frac{dp_A}{(P - p_A)}$$

$$N_A = \frac{D_{AB}}{(z_2 - z_1)} \frac{P}{RT} \ln \frac{P - p_{A2}}{P - p_{A1}}$$



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$$N_A = \frac{D_{AB}}{(z_2 - z_1)} \frac{P}{RT} \ln \frac{P - p_{A2}}{P - p_{A1}}$$

$$\text{Total Pressure (P)} = p_{A1} + p_{B1} = p_{A2} + p_{B2}$$

$$p_{B1} = P - p_{A1}$$

$$p_{B2} = P - p_{A2}$$

$$N_A = \frac{D_{AB}}{(z_2 - z_1)} \frac{P}{RT} \ln \frac{p_{B2}}{p_{B1}}$$

$$p_{BM} = \frac{p_{B2} - p_{B1}}{\ln \frac{p_{B2}}{p_{B1}}} = \frac{p_{A1} - p_{A2}}{\ln \frac{p_{B2}}{p_{B1}}}$$

*Log mean value of the Inert B*

$$N_A = \frac{D_{AB}}{(z_2 - z_1)} \frac{P}{RT} \frac{p_{A1} - p_{A2}}{p_{BM}}$$



## Molecular Diffusion in Gases-

### Special Case for A Diffusing Through Stagnant, Nondiffusing B

$$N_A = \frac{D_{AB}}{(z_2 - z_1)} \frac{1}{RT} \frac{P}{p_{BM}} (p_{A1} - p_{A2})$$

$$J_{Az}^* = \frac{D_{AB}}{(z_2 - z_1)} \frac{1}{RT} (p_{A1} - p_{A2})$$



## Your Turn

### Diffusion of Water Through Stagnant, Non-diffusing Air

Water in the bottom of a narrow metal tube is held at a constant temperature of 293 K. The total pressure of air (assumed dry) is  $1.01325 \times 10^5$  Pa (1.0 atm) and the temperature is 293 K (20°C). Water evaporates and diffuses through the air in the tube and the diffusion path ( $z_2 - z_1$ ) is 0.1524 m long. Calculate the rate of evaporation at steady state. The diffusivity of water vapor at 293 K and 1 atm pressure is  $0.250 \times 10^{-4}$  m<sup>2</sup>/s. Assume that the system is isothermal.



## References

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3. Middleman S., An Introduction to Mass and Heat Transfer: Principles of Analysis and Design, John Wiley, High Education, 1997.
4. Cussler E.L., Diffusion : Mass Transfer in Fluid Systems, Cambridge University Press, 3<sup>rd</sup> Edition, 2009.
5. Bird R.B., Stewart W.E., Lightfoot E.N., Transport Phenomena, John Wiley & Sons, 1960.

