

**CEN 3313**

**MASS TRANSFER**

**Assoc. Prof. Ayşe Karakeçili**

**Assoc. Prof. Berna Topuz**



# Molecular Diffusion in Gases-

## Interface Fall for A Diffusing Through Stagnant Film of B

$$\overline{N_A} = N_A \times Area$$

$$= \frac{\rho_A}{M_A} \frac{dz}{dt} \times Area$$

$$\frac{D_{AB}}{z} \frac{P}{RT} \frac{p_{A1} - p_{A2}}{p_{BM}} = \frac{\rho_A}{M_A} \frac{dz}{dt}$$

$$D_{AB} \frac{P}{RT} \frac{p_{A1} - p_{A2}}{p_{BM}} \int_0^{t_F} dt = \frac{\rho_A}{M_A} \int_{z_0}^{z_F} z dz$$

$$t_F = \frac{\rho_A}{M_A} \frac{(z_F^2 - z_0^2)}{2D_{AB}} \left( \frac{P}{RT} \frac{p_{A1} - p_{A2}}{p_{BM}} \right)^{-1}$$

$$(z_F^2 - z_0^2) = \left( \frac{P}{RT} \frac{p_{A1} - p_{A2}}{p_{BM}} \right) \left( \frac{M_A}{\rho_A} \right) (2D_{AB}) t_F$$



# Diffusion through a Varying Cross-Sectional Area

## a) Diffusion from a sphere

- Evaporation of a ball of naphthalene
- Evaporation of a drop of liquid
- Diffusion of nutrients from a spherical micro-organism

For spherical geometry,

$$N_A = \frac{\overline{N_A}}{4\pi r^2}$$



# Diffusion through a Varying Cross-Sectional Area: 1. Diffusion from a sphere

A Diffusing Through Stagnant, Nondiffusing B

$$N_A = \frac{\overline{N_A}}{4\pi r^2} = -D_{AB} \frac{P}{RT} \frac{1}{(P - p_A)} \frac{dp_A}{dr}$$



$$N_A \left(1 - \frac{p_A}{P}\right) = -\frac{D_{AB}}{RT} \frac{d(p_A)}{dz}$$

$$\frac{\overline{N_A}}{4\pi} \int_{r_1}^{r_2} \frac{dr}{r^2} = -D_{AB} \frac{P}{RT} \int_{p_{A1}}^{p_{A2}} \frac{1}{(P - p_A)} dp_A$$

$$\frac{\overline{N_A}}{4\pi} \left(\frac{1}{r_1} - \frac{1}{r_2}\right) = D_{AB} \frac{P}{RT} \ln \frac{P - p_{A2}}{P - p_{A1}}$$

For  $r_2 \gg r_1$ ,  $1/r_2 \rightarrow 0$

$$\frac{\overline{N_A}}{4\pi r_1} = D_{AB} \frac{P}{RT} \ln \frac{P - p_{A2}}{P - p_{A1}}$$

$$N_A = \frac{\overline{N_A}}{4\pi r_1^2} = \frac{D_{AB}}{r_1} \frac{P}{RT} \left[ \ln \frac{P - p_{A2}}{P - p_{A1}} \right] = \frac{D_{AB}}{r_1} \frac{P}{RT} \left[ \frac{p_{A1} - p_{A2}}{p_{BM}} \right]$$



# Diffusion through a Varying Cross-Sectional Area

## 2) Diffusion through a conduit of non-uniform cross-sectional area

$$r = \left( \frac{r_2 - r_1}{z_2 - z_1} \right) z + r_1$$

$$A = \pi r^2 = \pi \left[ \left( \frac{r_2 - r_1}{z_2 - z_1} \right) z + r_1 \right]^2$$

$$N_A = \frac{\overline{N_A}}{\pi r^2} = -D_{AB} \frac{P}{RT} \frac{1}{(P - p_A)} \frac{dp_A}{dr}$$

$$N_A = \frac{\overline{N_A}}{\pi} \int_{r_1}^{r_2} \frac{dz}{\left[ \left( \frac{r_2 - r_1}{z_2 - z_1} \right) z + r_1 \right]^2} = -D_{AB} \frac{P}{RT} \int_{p_{A1}}^{p_{A2}} \frac{1}{(P - p_A)} dp_A$$



## Your Turn

A sphere of naphthalene having a radius of 2 mm is suspended in a large volume of still air at 318K, and 1 atm. The surface temperature of naphthalene can be assumed to be 318K and its vapor pressure at 318K is 0.55 mm Hg.  $D_{AB} = 6.92 \times 10^{-6} \text{m}^2/\text{s}$ . Calculate the rate of evaporation of naphthalene from the surface.



## References

1. Geankoplis, C.J., Transport Processes and Separation Process Principles, Prentice-Hall, Pearson Education, 2003
2. Incropera F. P., Dewitt D. P. , Bergman T.L., Lavine A.S., Fundamentals of Heat and Mass Transfer, John Wiley & Sons Inc.
3. Middleman S., An Introduction to Mass and Heat Transfer: Principles of Analysis and Design, John Wiley, High Education, 1997.
4. Cussler E.L., Diffusion : Mass Transfer in Fluid Systems, Cambridge University Press, 3<sup>rd</sup> Edition, 2009.
5. Bird R.B., Stewart W.E., Lightfoot E.N., Transport Phenomena, John Wiley & Sons, 1960.

