

#### CEN4417 PROCESS DESIGN I

## **Tools for Evaluating Process Performance**

# Methods

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  - 5.3. The T-Q Diagram for Heat Exchanger

# **1. KEY RELATIONSHIPS**

 In analyzing equipment performance, there are certain key relationships that are used over and over again.

#### Table 17.1 Typical Key Performance Relationships

Situation	Equation	Trends	Comments
Frictional loss for fluid flow	$\Delta P = \frac{2 g R_{eq} \mu^2}{D}$	$ \begin{aligned}  \Delta P  &\propto u^2 \\  \Delta P  &\propto D^{-5} \\  \Delta P  &\propto L \end{aligned} $	Assumes fully developed turbulent flow, i.e., constant friction factor; for laminar flow $\Delta P \approx D^{-4}$ .
Heat transfer	Of form $\left(\frac{hD}{k}\right) = c \left(\frac{Dn\rho}{\mu}\right)^{\mu} \left(\frac{\mu C_{\mu}}{k}\right)^{\mu}$	$h_i \propto v^{0.8}$ inside closed channels $h_o \propto v^{0.6}$ cross flow outside pipes	Equations given are for no phase change; if phase change, weak flow dependence, but some $\Delta T$ dependence.
Kinetics	$r = k \prod c_i^{a_i}$ $k = k_i e^{-\left(\frac{k_i}{Kt}\right)}$	$\ln k$ vs 1/T is linear	As $T \uparrow, k \uparrow$ for ideal gases $P \uparrow, c_i \uparrow$ , so $r \uparrow$ .
Reactor	mixed flow: $\frac{V}{F_{A0}} = \frac{\tau}{C_{A0}} = \frac{X}{-r_A}$ plug flow: $\frac{V}{F_{A4}} = \frac{\tau}{C_{A0}} = \int_{0}^{N} \frac{dX}{-r_A}$	τ ∝V as τ ↑ or V ↑, X ↑	τ is space time, V is reactor volume, X is conversion of limiting reactant, A assumes one reac- tion and constant volumetric flowrate.
Separator using mass separating agent	Not necessarily described by a single equation	As flow of mass separ- ating agent 1, or as number stages or height of packed tower 1, degree of separation 1	For certain cases, there are limitations to the ef- fect of increasing num- ber of stages or packed tower height.
Distillation	Not necessarily described by a single equation	As reflux ratio $\hat{T}$ , degree of separation $\hat{T}$	Complicated analysis; see Chapter 18.

# **2.Thinking with Equations**

- It is possible to quantify equipment performance without resorting to extensive, detailed calculations.
- This involves using equations to understand trends.
- The first step is to identify the equations necessary to quantify a given situation.
- Wales and Stager have termed this "thinking with equations" and have used the acronym GENI to describe the associated problem-solving strategy.
- The second step involves predicting trends from equations. These methods are described and then illustrated in an example.

# 2.1. GENI

GENI is a method for solving quantitative problems.

**1. Goal**: Identify the goal.

**2. Equation**: Identify the equation that relates the unknown to known values or properties.

**3. Need**: Identify additional relationships that are needed to solve the equation in Step 2.

**4. Information**: List additional information that is available to determine whether what is needed in Step 3 is known

### REFERENCES

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 Chemical Engineering Design, ButterWorth Heinemann, Oxford.

2. Turton R., Bailie R.C., Whitin W.C., Shaeiwitz J.A. 1998, Analysis, Synthesis and Design of Chemical Processes, Prentice Hall, New Jersey.