

References:

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10. Heating and cooling of fluids in forced convection outside tubes :

Cross-flow over a cylinder

$$T_{\infty} = 30 \text{ }^{\circ}\text{C}, \quad T_w = 324 \text{ }^{\circ}\text{C}$$

$$T_f = \frac{T_w + T_{\infty}}{2} = \frac{324 + 30}{2} = 177^{\circ}\text{C} = 450 \text{ K}$$

Physical properties of air at 450 K (Table 5) : $\rho = 0.7833 \text{ kg/m}^3$

$$\mu = 2.484 \times 10^{-5} \text{ kg/ms}$$

$$k = 0.03707 \text{ W/m}^{\circ}\text{C}$$

$$\text{Pr} = 0.683$$

$$\frac{hD}{k} = c \left(\frac{D_o V_{\infty} \rho_f}{\mu_f} \right)^n \text{Pr}^{1/3}$$

$$\text{Re}_f = \frac{D_o V_{\infty} \rho_f}{\mu_f} = \frac{3 \times 10^{-3} \text{ m} \times 6 \text{ m/s} \times 0.7833 \text{ kg/m}^3}{2.484 \times 10^{-5} \text{ kg/ms}} = 567$$

$$\text{Re}_f = 567 \text{ (range } 40 - 4000) \quad c=0.683 \quad n=0.466 \text{ (from Table 12)}$$

$$\frac{h \times 3 \times 10^{-3} \text{ m}}{0.03707 \text{ W/m}^{\circ}\text{C}} = 0.683 (567)^{0.466} (0.683)^{1/3} = 11.54 \rightarrow h = 142.66 \frac{\text{W}}{\text{m}^2\text{ }^{\circ}\text{C}}$$

$$q = h * A * (T_w - T_{\infty})$$

$$q = h * \pi D L * (T_w - T_{\infty})$$

$$\frac{q}{L} = h * \pi D * (T_w - T_{\infty}) = 142.66 \frac{\text{W}}{\text{m}^2\text{ }^{\circ}\text{C}} * \pi * 3 \times 10^{-3} \text{ m} * (324 - 30)^{\circ}\text{C}$$

$$\frac{q}{L} = 395.3 \frac{\text{W}}{\text{m}}$$

Example:

An in-line arrangement cross flow heat exchanger is set up 6 rows parallel to the flow and 4 rows normal to the flow. $L = 15.24$ m $D = 0.0064$ m and $S_n = S_p = 0.0192$ m. $T_w = 93.3$ °C. Atmospheric air, velocity of 4.57 m/s, is heated in the system

$$\bar{T} = 21.1^\circ\text{C}$$

$$T_f = \frac{T_w + \bar{T}}{2} = \frac{93.3 + 21.1}{2} = 57.2^\circ\text{C} = 330.2\text{ K}$$

The properties of air at 330.2 K by interpolation:

$$\rho_f = 1.0656\text{ kg/m}^3$$

$$\mu_f = 1.9844 \times 10^{-5}\text{ kg/m}\cdot\text{s}$$

$$k_f = 0.02853\text{ W/m}\cdot^\circ\text{C}$$

$$C_p = 1.0077\text{ kJ/kg}\cdot^\circ\text{C}$$

$$\text{Pr} = 0.701$$

$$\theta_{\max} = \theta_\infty \frac{S_n}{S_n - D} = 4.57 \frac{0.0192}{0.0192 - 0.0064} = 6.86\text{ m/s}$$

$$\text{Re} = \frac{D \theta_{\max} \rho}{\mu} = \frac{0.0064 \times 6.86 \times 1.0656}{1.9844 \times 10^{-5}} = 2357.6$$

$$\text{Nu} = c \left(\frac{D \theta_{\max} \rho}{\mu} \right)^n \text{Pr}^{1/3}$$

The constants (c and n) are obtained from Table 13, using

$$\frac{S_p}{D} = \frac{S_n}{D} = \frac{0.0192}{0.0064} = 3$$

$$c = 0.317$$

$$n = 0.608$$

$$\frac{h \times 0.0064}{0.02853} = 0.317 \times (2357.6)^{0.608} \times (0.701)^{\frac{1}{3}}$$

$$h = 141\text{ W/m}^2\cdot^\circ\text{C}$$

This h is for ten rows. There are only 6 rows in this system. This value must be multiplied by the factor 0.94, as determined from Table 14.

$$h = 141 \times 0.94 = 132.54\text{ W/m}^2\cdot^\circ\text{C}$$

$$A = \pi D L \times N = \pi \times 0.0064 \times 15.24 \times 24 = 7.354\text{ m}^2$$

$$q = hA(T_w - \bar{T}) = 132.54 \times 7.354 \times 72.2 = 70373.3\text{ W}$$