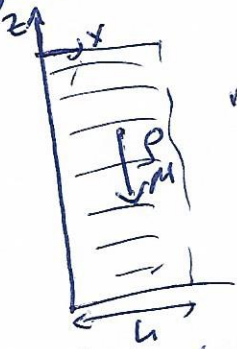


exp.

consider steady incompressible laminar flow of a film of viscous liquid falling down on a vertical wall. The film thickness is "h" and gravity acts in the negative "z" direction. There is no applied pressure driving the flow - the liquid falls by gravity alone. Calculate the velocity profile in the film! You might assume negligible shear on the outer surface of the film. (free-surface!)



$p = p_{atm}$

Continuity equation

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0 \Rightarrow \frac{\partial w}{\partial z} = 0$$

no-flow in x-y directions.

$$\frac{\partial w}{\partial y} = 0 \text{ (no flow in y)}$$

$$\frac{\partial w}{\partial t} \neq 0$$

$D = v = 0$

$p_x = p_y = 0$  only flow in z-direction.

no-flow in x and y directions! only -z-

$$\rho \left( \frac{\partial u}{\partial t} + \frac{\partial u}{\partial x} \frac{\partial w}{\partial z} + \frac{\partial v}{\partial y} \frac{\partial w}{\partial z} + w \frac{\partial u}{\partial z} \right) = - \frac{\partial p}{\partial z} + \rho g$$

$\rightarrow$  (continuity)  $\rightarrow$   $\rho g$

$$+ \mu \left( \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial z^2} + \frac{\partial^2 v}{\partial y^2} \right) = 0$$

no pressure gradient!

$$\mu \frac{\partial^2 w}{\partial z^2} = \rho g = 0$$

$$\mu \frac{dw}{dz} = \rho g$$

$$\frac{dw}{dz} = \frac{\rho g}{\mu}$$

$$w = \frac{\rho g}{\mu} z + C_1$$

B-C, no-slip.

$$w(0) = 0 \Rightarrow c_2 = 0$$

$$\left. \frac{dw}{dx} \Big|_{x=h} = 0 \quad \left\{ \text{negligible shear!} \right\} \left\{ \begin{array}{l} \tau = 0 \\ -\mu \frac{dw}{dx} = 0 \end{array} \right\}$$

$$\frac{dw}{dx} \Big|_{x=h} = \frac{\rho g}{\mu} \cdot h + c_1 = 0$$

$$c_1 = -\frac{\rho g}{\mu} \cdot h$$

$$w(x) = \frac{\rho g}{\mu} \frac{x^2}{2} - \frac{\rho g h}{\mu} x$$

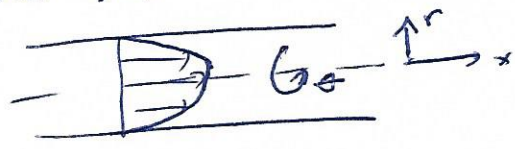
$$w(x) = \frac{\rho g x}{2\mu} (x - 2h)$$

Since  $x < h$  in the film,

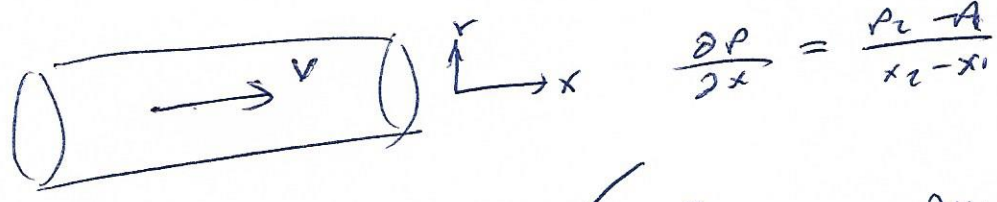
$w$  is "—" as expected!

ex

Consider steady, incompressible <sup>(laminar parallel)</sup> flow of a Newtonian fluid in a pipe where  $\mu = 0.1$  ignoring the effects of gravity. If a constant pressure gradient is applied in the x-direction, derive an expression for the velocity inside the pipe.



continuity:  $\frac{1}{r} \frac{\partial (r u_r)}{\partial r} + \frac{1}{r} \frac{\partial (u_\theta)}{\partial \theta} + \frac{\partial u_x}{\partial x} = 0$



parallel flow  $u_r = 0$  ✓  
 no swirl  $u_\theta = 0$  ✓

$\Rightarrow \frac{\partial u_x}{\partial x} = 0$   
 $u$  is not a function of  $x$ !  
 axis-symmetric in  $\theta$ !  
 so,  $u = f(r)$ .

x-direction

Steady  $u_r = 0$

$$\rho \left( \frac{\partial u_x}{\partial t} + u_r \frac{\partial u_x}{\partial r} + \frac{u_\theta}{r} \frac{\partial u_x}{\partial \theta} + \frac{u_x}{r} \frac{\partial u_x}{\partial x} \right) = -\frac{\partial p}{\partial x} + \mu \left[ \frac{1}{r} \frac{\partial}{\partial r} \left( r \frac{\partial u_x}{\partial r} \right) + \frac{\partial^2 u_x}{\partial z^2} \right]$$

$$-\frac{\partial p}{\partial x} + \mu \left( \frac{1}{r} \frac{\partial}{\partial r} \left( r \frac{\partial u_x}{\partial r} \right) \right) = 0$$

$u = f(r)$

$$\frac{1}{r} \frac{d}{dr} \left( r \frac{du}{dr} \right) = \frac{1}{\mu} \frac{dp}{dx}$$

$$r \frac{dU}{dr} = \frac{r^2}{4\mu} \cdot \frac{dP}{dx} + C_1$$

$$U(r) = \frac{r^2}{4\mu} \cdot \frac{dP}{dx} + C_1 \ln(r) + C_2$$

$$\text{At } r=0 \quad \frac{\partial U}{\partial r} = 0 \quad \text{axis-symmetry!} \quad \Rightarrow$$

$$C_1 = \underline{\underline{0}}$$

$$r=R \quad U(r=R) = 0$$

$$\frac{R^2}{4\mu} \cdot \frac{dP}{dx} + C_2 = 0 \Rightarrow$$

$$C_2 = -\frac{R^2}{4\mu} \cdot \frac{dP}{dx}$$

$$U(r) = \frac{r^2}{4\mu} \cdot \frac{dP}{dx} + \frac{R^2}{4\mu} \cdot \frac{dP}{dx}$$

$$U(r) = \frac{1}{4\mu} \cdot \frac{dP}{dx} (r^2 - R^2) \quad \checkmark$$