

# Example 3: Isothermal CSTR with 1. Order Chemical Reaction

Find the model and the transfer function of the process.

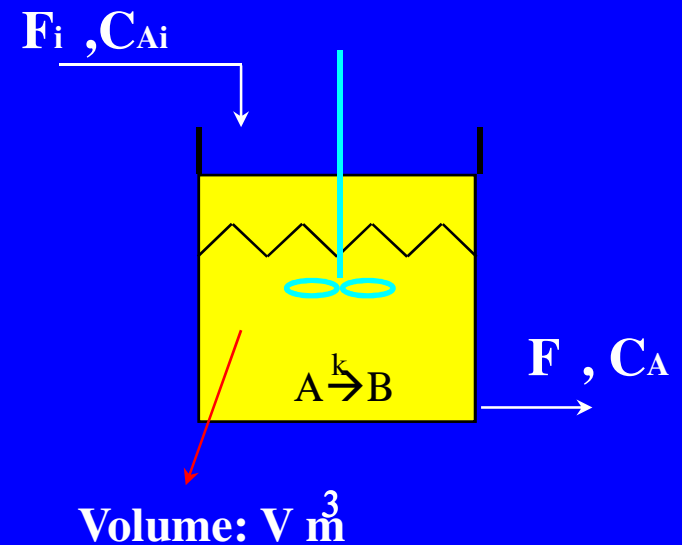
Mass balance for component A

Accumulation = In - Out + Generation

$$\frac{d(M_A V C_A)}{dt} = M_A F C_{Ai} - M_A F C_A - M_A V k C_A$$

$M_A$ : molecular weight of A,  $V = \text{constant}$

$$\frac{dC_A}{dt} = \frac{F}{V} C_{Ai} - \frac{F}{V} C_A - k C_A$$



Output var.:  $C_A$  (mol/m<sup>3</sup>)

Input var.:  $C_{Ai}$  (mol/m<sup>3</sup>)

$$\frac{dC_A}{dt} + \left( \frac{F + kV}{V} \right) C_A = \frac{F}{V} C_{Ai}$$

**Model:**

$$\tau \frac{dC_A}{dt} + C_A = \frac{F}{F + kV} C_{Ai}$$

$\frac{V}{F + kV}$

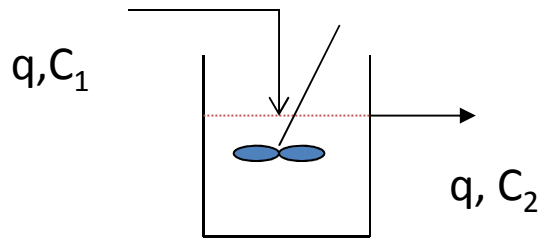
Take laplace , [  $C_A(t=0) = 0$  initial condition ]

$$\tau s C_A(s) + C_A(s) = \frac{F}{F + kV} C_{Ai}(s)$$

Transfer Function:

$$G(s) = \frac{C_A(s)}{C_{Ai}(s)} = \frac{K}{\tau s + 1}$$

# Example 4: Mixing



$V$ : volume of tank( $m^3$ )

$q$ : volumetric flow rate( $m^3 / s$ )

$C_1$  : inlet sugar conc.( $kg/m^3$ )

$C_2$  : outlet sugar conc.( $kg/m^3$ )

**Find the model and the transfer function of this process**

$C_1$  : input variable (in terms of deviation variable)

$C_2$  : output variable (in terms of deviation variable)

What is the transfer function of the process:  $\frac{C_2(s)}{C_1(s)} = ?$

Mass Balance:

Rate of mass in–Rate of mass out= Rate of Mass Accum.

$$\dot{m}_{in} - \dot{m}_{out} = \frac{d(m)}{dt}$$

$$qC_1 - qC_2 = \frac{d(VC_2)}{dt}$$

$$q(C_1 - C_2) = V \frac{d(C_2)}{dt}$$

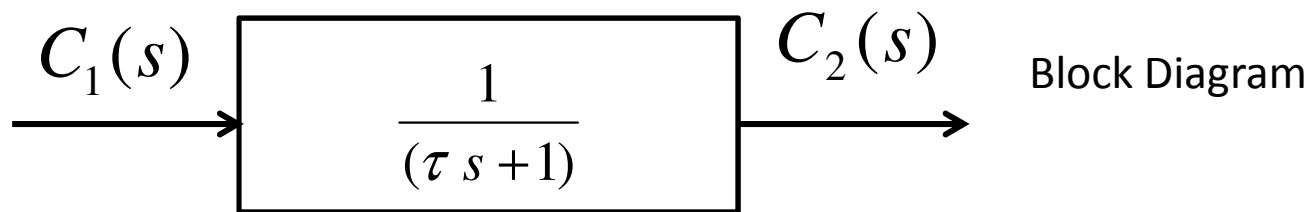
$$(C_1 - C_2) = \underbrace{\left(\frac{V}{q}\right)}_{\tau} \frac{d(C_2)}{dt}$$

$$C_1 = \tau \frac{d(C_2)}{dt} + C_2$$

$$C_1(s) = \tau s C_2(s) + C_2(s)$$

$$C_1(s) = C_2(s) [\tau s + 1]$$

$$\frac{C_2(s)}{C_1(s)} = \frac{1}{[\tau s + 1]}$$



# Example 5: If there are two input variables

In some cases there may be two input variables effecting the process. (Example: mixing tank with two inlet streams)

$$\tau \frac{dy}{dt} + y = x$$

**Mathematical model of a process that is represented by a 1st order differential equation (single input variable)**

$$\tau \frac{dy}{dt} + y = K_1 x_1 + K_2 x_2$$

**Mathematical model of a process that is represented by a 1st order differential equation (two input variables)**

y: output variable

x: input variable

$\tau$  : (tau) time constant

K: gain  $\rightarrow$  constant

# Example 5: If there are two input variables

Let's find the transfer function of this process. (take laplace)

$$\tau \frac{dy}{dt} + y = K_1 x_1 + K_2 x_2$$

$$\tau sY(s) - y(0) + Y(s) = K_1 X_1(s) + K_2 X_2(s)$$

$$Y(s) [\tau s + 1] = K_1 X_1(s) + K_2 X_2(s)$$

$$Y(s) = \frac{K_1}{[\tau s + 1]} X_1(s) + \frac{K_2}{[\tau s + 1]} X_2(s)$$

$$\frac{Y(s)}{X_1(s)} = \frac{K_1}{[\tau s + 1]}$$

$$\frac{Y(s)}{X_2(s)} = \frac{K_2}{[\tau s + 1]}$$

# Example 5: If there are two input variables

$$\frac{Y(s)}{X_1(s)} = \frac{K_1}{[\tau s + 1]}$$

**Transfer function I**

$$\frac{Y(s)}{X_2(s)} = \frac{K_2}{[\tau s + 1]}$$

**Transfer function II**

Y(s) is equal to sum of these two transfer functions

