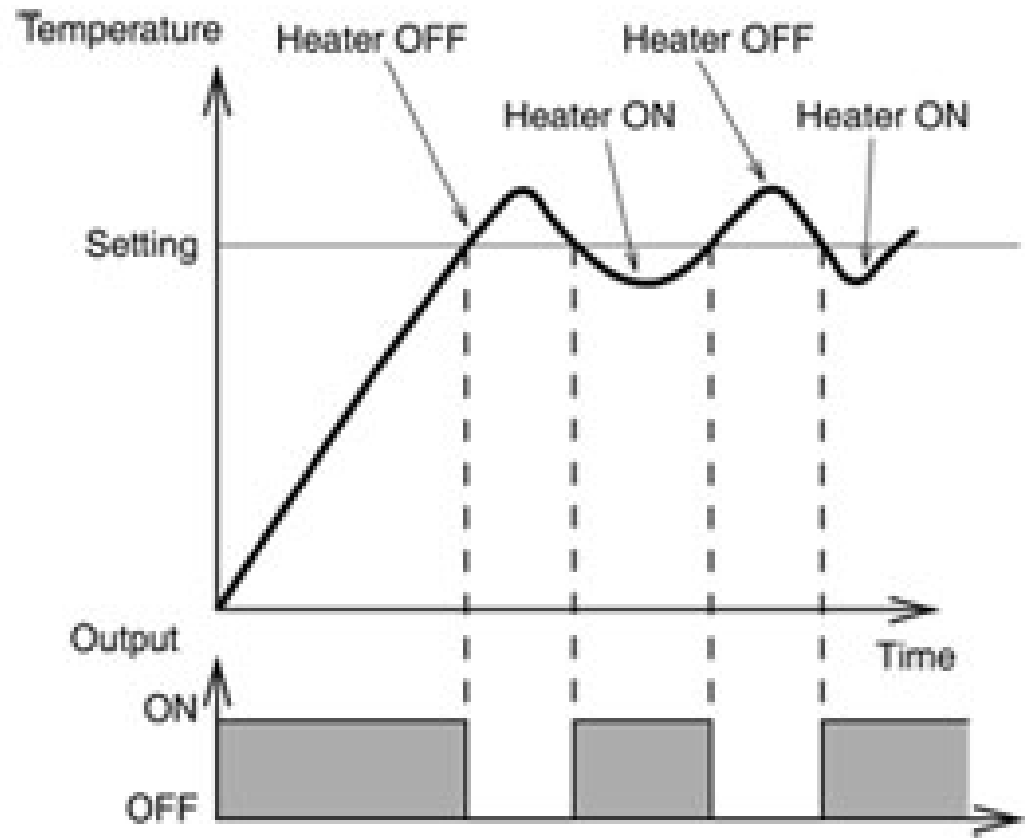


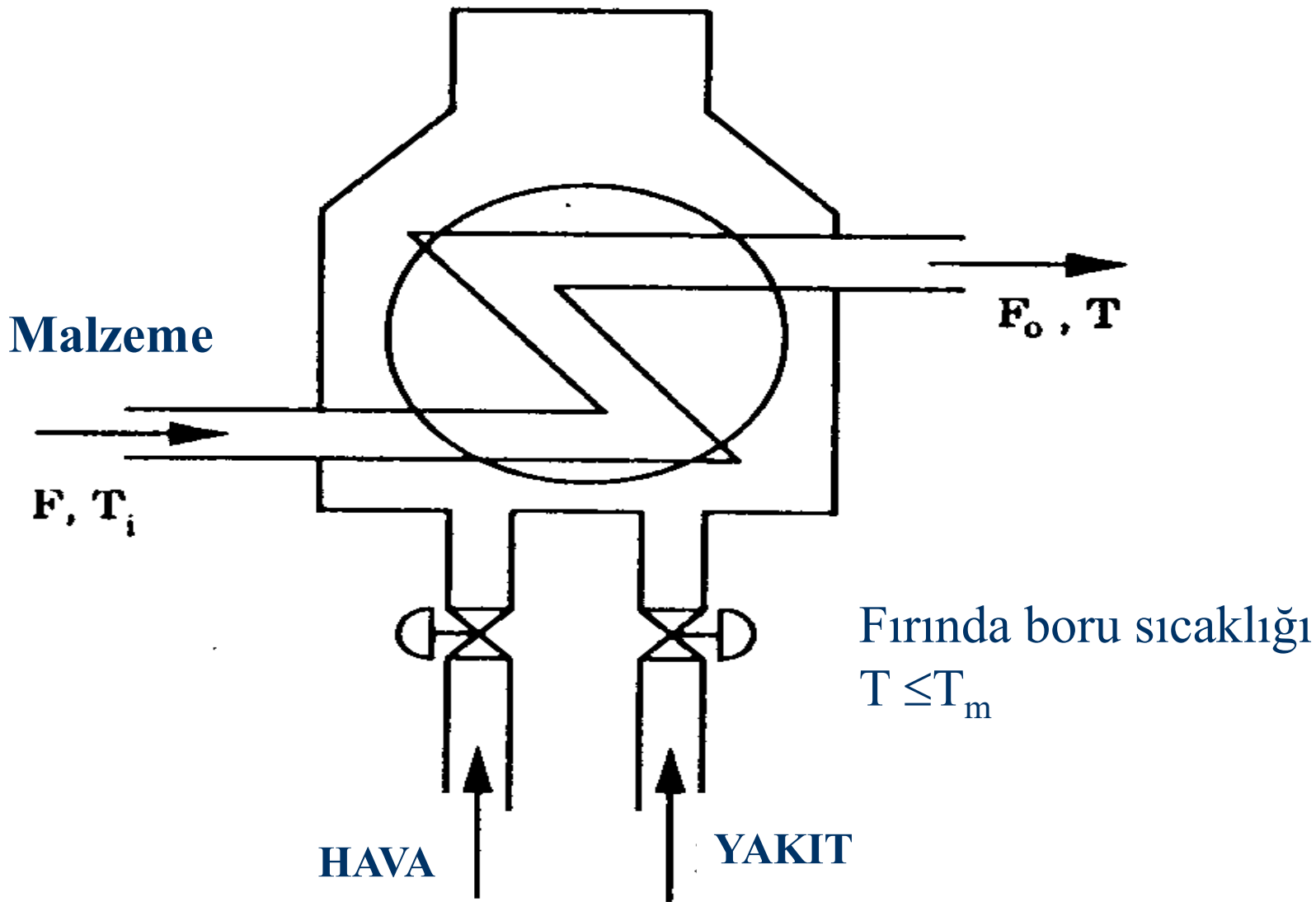
Bölüm 6. KONTROL SİSTEMLERİNİN SINIFLANDIRILMASI

- 👉 **Klasik** : Geri beslemeli kontrol
- 👉 **Gelişmiş Klasik Kontrol** : Ölü zaman dengeleme
 - İleri besleme kontrol
 - Kaskad(*cascade*) kontrol
- 👉 **Model Esaslı Kontrol** : Model öngörmeli kontrol
 - Optimal kontrol

Aç-Kapa (On-Off) kontrol cihazıyla kontrol edilen bir sistemin, sıcaklık zaman eğrisi görülmektedir.

ON/OFF Control



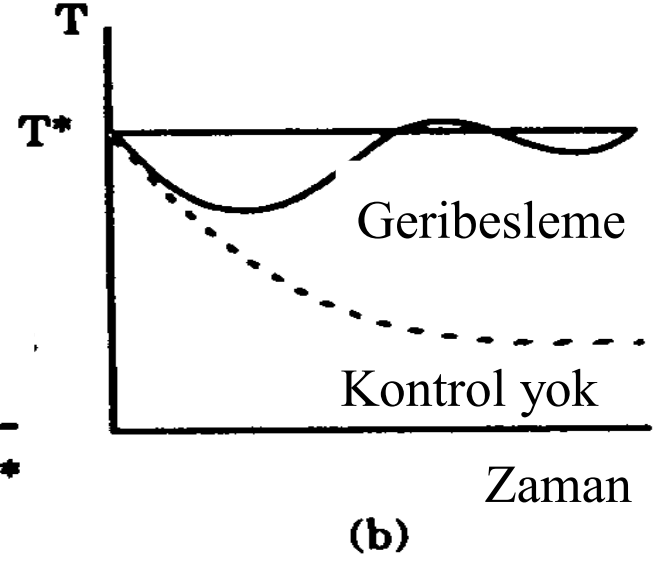
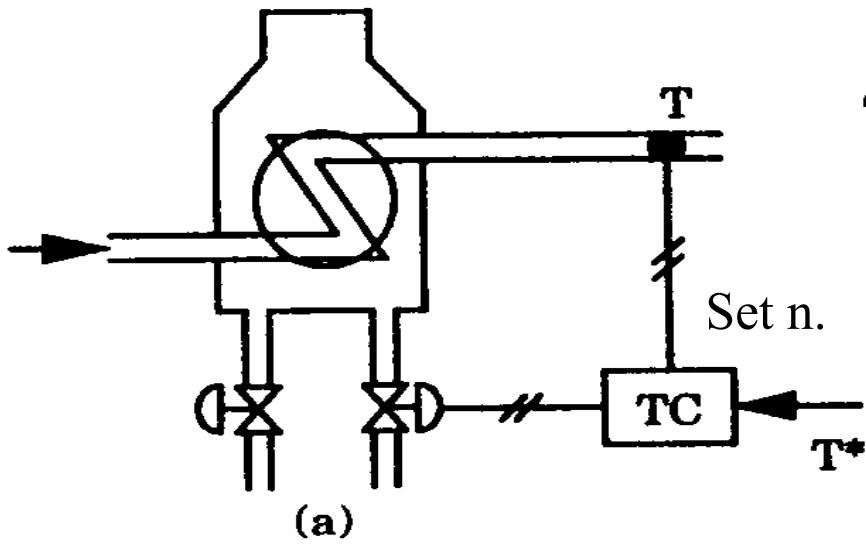


$Q_A =$ Hava akış hızı

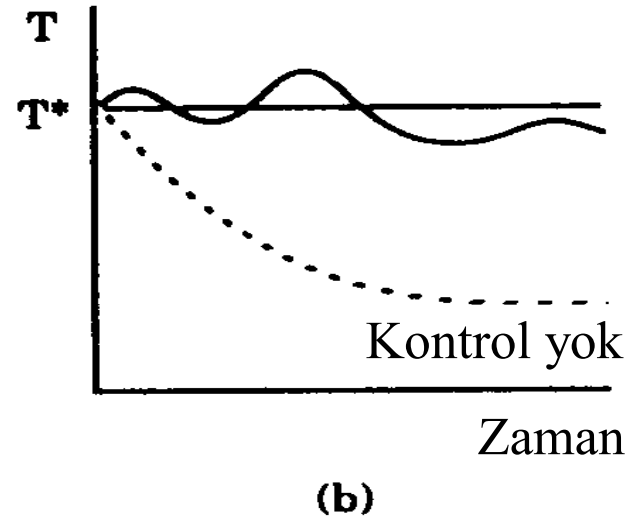
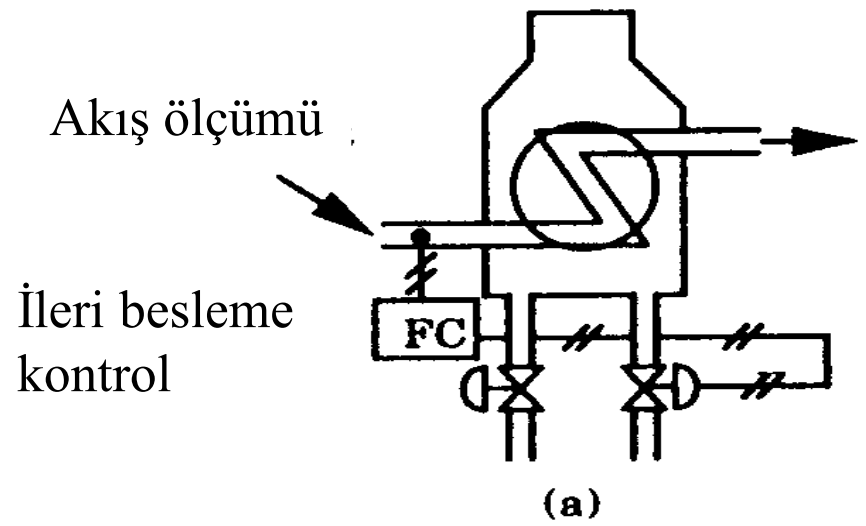
$Q_F =$ Yakıt akış hızı

$P_F =$ Yakıtın giriş basıncı

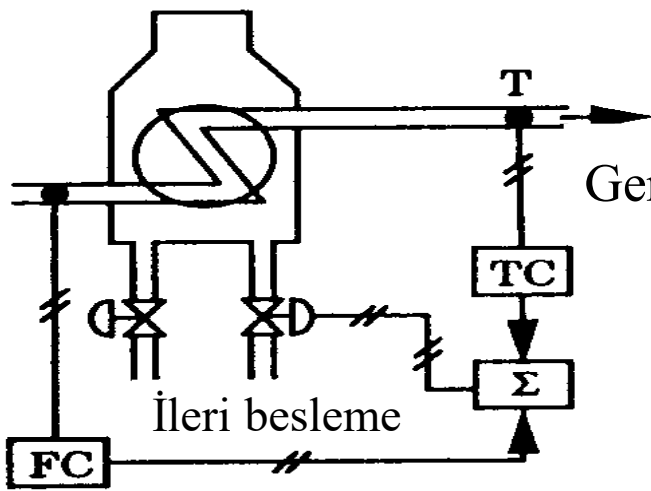
$\lambda_F =$ Yakıtın ısı kapasitesi



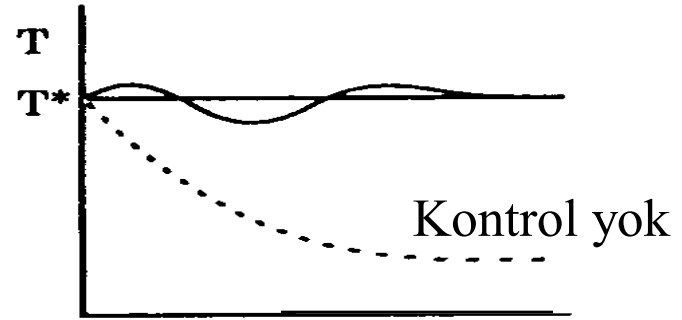
Geri besleme kontrol sistemi



İleri besleme kontrol sistemi

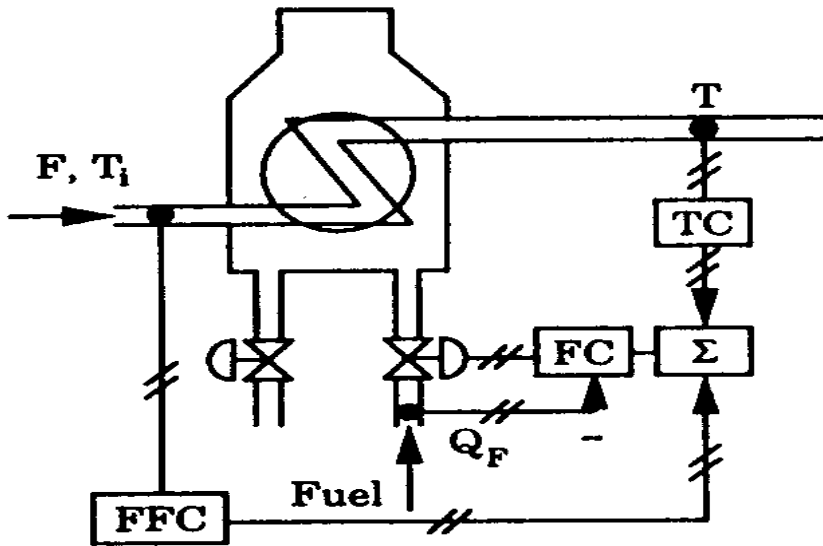


(a)

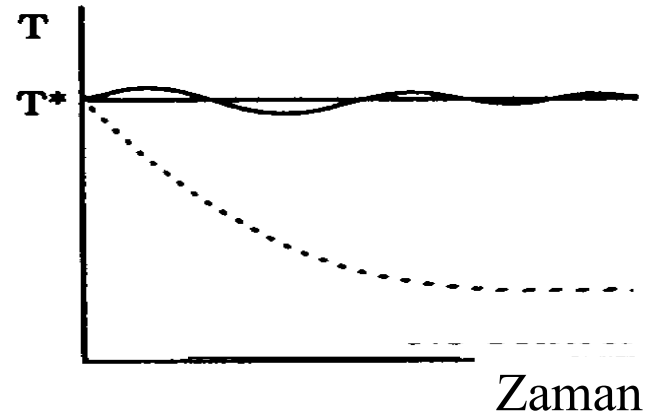


(b) Zaman

İleri besleme/geri besleme kontrol sistemi



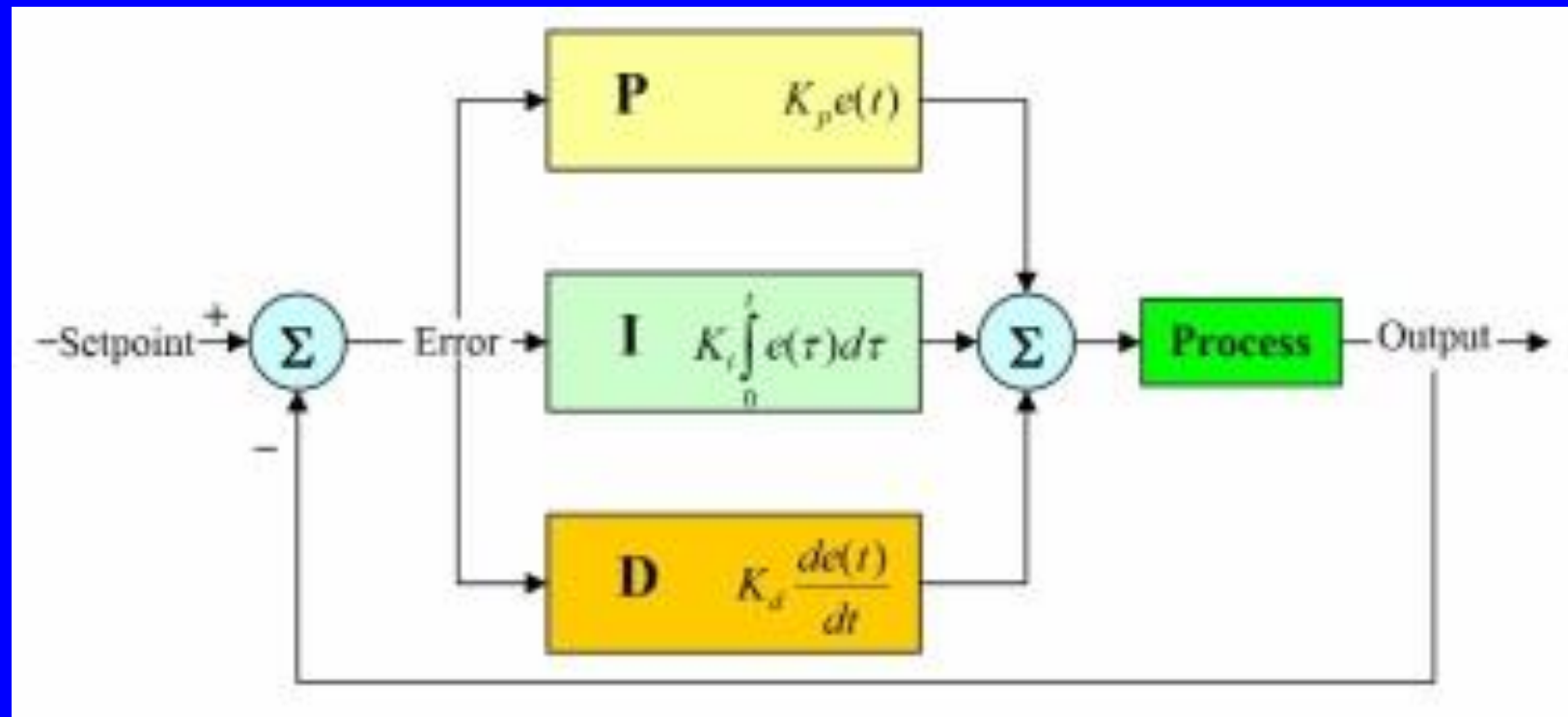
(a)



(b)

Son kontrol sistemi (İleri/geri/kaskad)

PROPORTIONAL - INTEGRAL - DERIVATIVE



Bölüm 7. BİRİNCİ VE İKİNCİ MERTEBE SİSTEMLERİN AÇIK DEVRE DİNAMİK DAVRANIŞI

Proses dinamiğini belirlemede kullanılan tipik girdiler;

$$\otimes \mathbf{x}_s(t) = \begin{cases} \mathbf{0} & t < 0 \\ \mathbf{A} & t \geq 0 \end{cases}$$

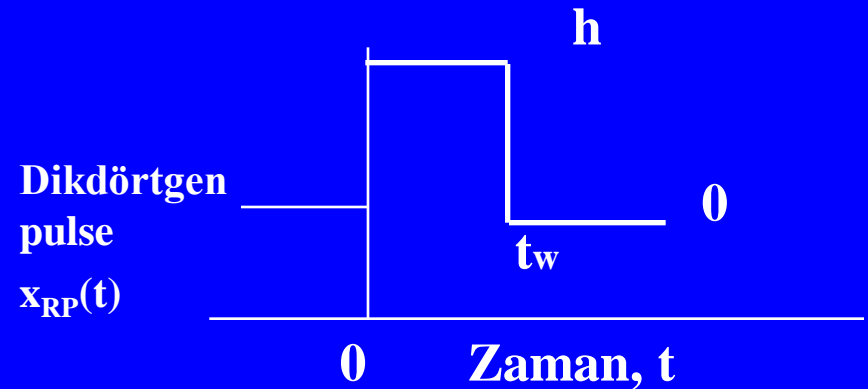
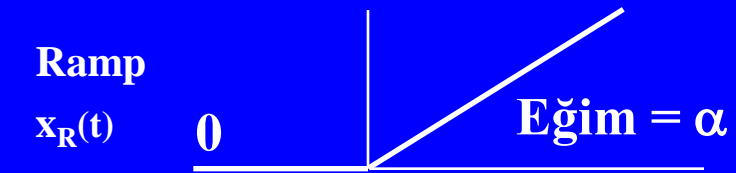
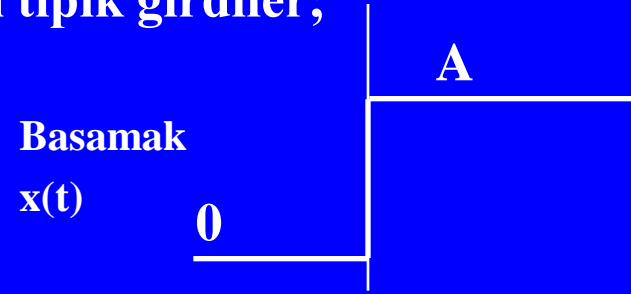
$$\mathbf{x}(s) = \mathbf{A}/s$$

$$\otimes \mathbf{x}_R(t) = \begin{cases} \mathbf{0} & t < 0 \\ at & t \geq 0 \end{cases}$$

$$\mathbf{x}_R(s) = a / s^2$$

$$\otimes \mathbf{x}_{RP}(t) = \begin{cases} \mathbf{0} & t < 0 \\ \mathbf{h} & 0 \leq t < t_w \\ \mathbf{0} & t > t_w \end{cases}$$

$$\mathbf{x}_{RP}(s) = \frac{\mathbf{h}}{s} (1 - e^{-t_w s})$$



7.1 Birinci Mertebe Sistemler

Basamak girdiye yanıtım

Karıştırmalı tankın ısıtılması örneğini ele alalım (*Örnek 8 s 63*) ;

Orijinal
$$\frac{dT}{dt} = \frac{F}{V} (T_i - T) + \lambda \frac{q}{\rho V C_p}$$

Sapma Değişkeni
$$\frac{dy}{dt} + \frac{F}{V} y = \frac{\lambda}{\rho V C_p} u + \frac{F}{V} d$$

t alanı

$$Y = T - T_s, \quad u = q - q_s, \quad d = T_i - T_{is}$$

Laplace
$$y(s) = \frac{K}{\tau s + 1} u(s) + \frac{1}{\tau s + 1} d \quad ; \quad \tau = \frac{V}{F}, \quad K = \frac{\lambda}{\rho F C_p}$$

s alanı

Girdi:

$$\mathbf{u}(t) = \begin{cases} \mathbf{0} & t < 0 \\ \mathbf{A} & t \geq 0 \end{cases} ; \quad \mathbf{u}(s) = \frac{\mathbf{A}}{s}$$

Yanıtım, diferansiyel denklemler çözülerek veya transfer fonksiyonundan bulunabilir.

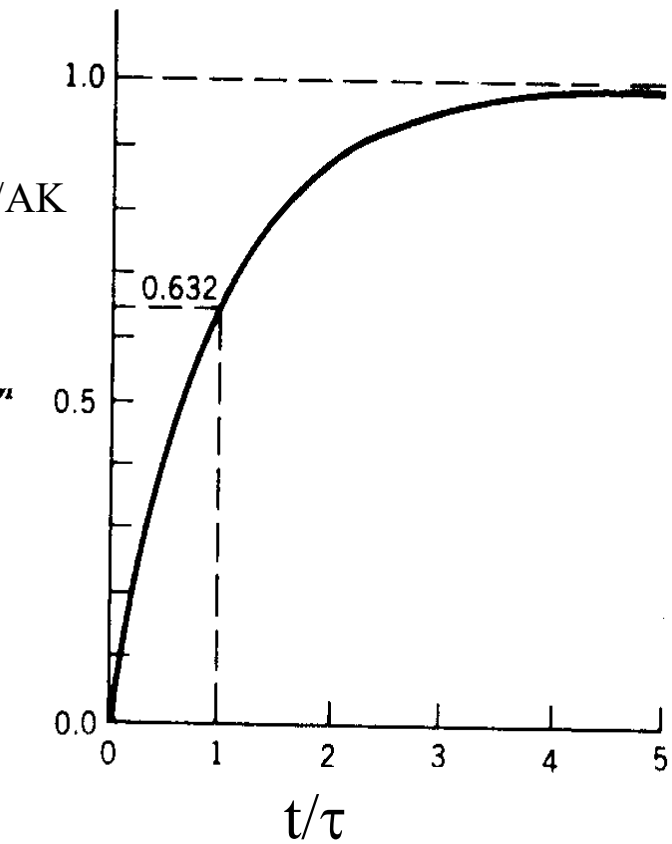
$$\mathbf{y}(s) = \frac{\mathbf{K}}{\tau s + 1} \frac{\mathbf{A}}{s}$$

Kısmi fraksiyonlama ile

$$\mathbf{y}(s) = \mathbf{AK} \left(\frac{1}{s} - \frac{\tau}{\tau s + 1} \right)$$

Her iki tarafın ters \mathcal{L} dönüşümü alınırsa,

$$\mathcal{L}^{-1}[\mathbf{y}(s)] = \mathbf{AK} \mathcal{L}^{-1} \left(\frac{1}{s} - \frac{\tau}{\tau s + 1} \right)$$
$$\mathbf{y}(t) = \mathbf{AK} \left(1 - e^{-t/\tau} \right)$$



Birinci mertebe prosesin
basamak tepkisi

$$y = KA(1 - e^{-\frac{t}{\tau}})$$

Birinci mertebe bir prosesin
basamak girdiye tepkisi

t	$y(t)/\frac{K}{A}$
0	0
τ	0.6321
2τ	0.8647
3τ	0.9502
4τ	0.9817
5τ	0.9933

