

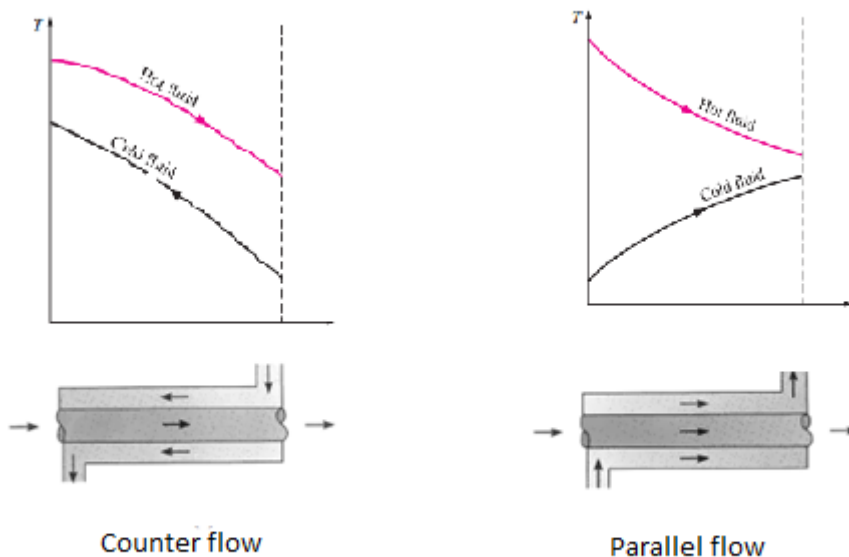
References:

- W.L. McCabe, J.C. Smith, P. Harriott., *Unit Operations of Chemical Engineering*, McGraw Hill, N.Y., (7th Ed.) 2005
- J.P. Holman, *Heat Transfer*, McGraw-Hill, N.Y., 1989.
- F.P. Incropera, D.P. de Witt, *Fundamentals of Heat and Mass Transfer*, John Wiley & Sons, N.Y., (3th Ed.) 1990.
- C.J. Geankoplis, *Transport Processes and Unit Operations*, Prentice-Hill Inc., N.J., (3th Ed.) 1993
- Y. Cengel , *Introduction to Thermodynamics and Heat Transfer* , , McGraw Hill, 2nd Edition 2008

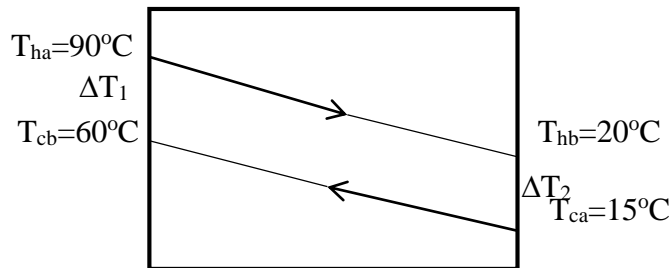
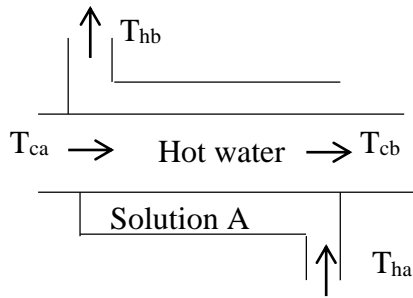
4. Principles of heat flow in fluids, typical heat exchange equipment

The general function of a heat exchanger is to transfer heat from one fluid to another. The basic component of a heat exchanger can be viewed as a tube with one fluid running through it and another fluid flowing by on the outside. There are thus three heat transfer operations that need to be described:

- 1) Convective heat transfer from fluid to the inner wall of the tube
- 2) Conductive heat transfer through the tube wall
- 3) Convective heat transfer from the outer tube wall to the outside fluid



Example:



$$\bar{T}_h = \frac{90 + 20}{2} = 55^\circ C \approx 54.44^\circ C$$

$$\bar{T}_c = \frac{60 + 15}{2} = 37.5^\circ C \approx 37.78^\circ C$$

Table 8

$$C_{ph} = 4.179 \text{ kJ}/(\text{kg}\cdot\text{C}), \quad \rho_h = 985.7 \text{ kg}/\text{m}^3 \quad \mu_h = 5.13 \frac{\text{kg}}{\text{ms}} \quad k_h = 0.649 \text{ W}/\text{m}^\circ\text{C}$$

$$C_{pc} = 0.941 \frac{\text{kcal}}{\text{kg}^\circ\text{C}} \times \frac{4.18 \text{ J}}{1 \text{ cal}} = 3.93 \frac{\text{kJ}}{\text{kg}^\circ\text{C}}$$

Table 8

$$\rho_c = 993 \text{ kg}/\text{m}^3 \quad \mu_c = 6.82 \frac{\text{kg}}{\text{ms}} \quad k_c = 0.63 \text{ W}/\text{m}^\circ\text{C}$$

Table 10

$$2 \text{ in sch 40 } D_o = 2.375 \text{ in} \quad D_i = 2.067 \text{ in}$$

$$D_o = 2.375 \text{ in} \frac{2.54 \text{ cm}}{1 \text{ in}} \frac{1 \text{ m}}{100 \text{ cm}} = 0.0603 \text{ m}$$

$$D_i = 2.067 \text{ in} \frac{2.54 \text{ cm}}{1 \text{ in}} \frac{1 \text{ m}}{100 \text{ cm}} = 0.052 \text{ m}$$

$$4 \text{ in sch 40 } D_o = 4.5 \text{ in} = 0.11 \text{ m} \quad D_i = 4.026 \text{ in} = 0.102 \text{ m}$$

$$q = m_c C_{pc} (T_{cb} - T_{ca}) = 200 \text{ kg}/\text{h} \times 3.93 \text{ kJ}/(\text{kg}^\circ\text{C}) (60 - 15)^\circ\text{C} = 35370 \text{ kJ}/\text{h}$$

$$q = 35370 \text{ kJ}/\text{h} \times 1000 \text{ J}/\text{kJ} \times 1 \text{ h}/3600 \text{ s} = 9825 \text{ J}/\text{s}$$

$$35370 \text{ kJ}/\text{h} = m_h \times 4.179 \text{ kJ}/(\text{kg}\cdot\text{C}) (90 - 20)^\circ\text{C}$$

$$m_h = 120.9 \text{ kg/h}$$

$$\Delta T_L = \frac{\Delta T_1 - \Delta T_2}{\ln \frac{\Delta T_1}{\Delta T_2}} = \frac{(T_{ha} - T_{cb}) - (T_{hb} - T_{ca})}{\ln \frac{T_{ha} - T_{cb}}{T_{hb} - T_{ca}}}$$

$$\Delta T_L = \frac{(90 - 60) - (20 - 15)}{\ln \frac{90 - 60}{20 - 15}} = 13.95^\circ \text{C}$$

$$U_o = \frac{1}{\frac{D_o}{D_i h_i} + \frac{x_w}{k_m} \frac{D_o}{D_L} + \frac{1}{h_o}}$$

$$\overline{D}_L = \frac{D_o - D_i}{\ln \frac{D_o}{D_i}} = \frac{0.0603 - 0.052}{\ln \frac{0.0603}{0.052}} = 0.056 \text{ m}$$

$$D_o = 0.0603 \text{ m}$$

$$D_i = 0.052 \text{ m}$$

$$\overline{D}_L = 0.056 \text{ m}$$

$$x_w = \frac{D_o - D_i}{2} = \frac{0.0603 - 0.052}{2} = 0.0041$$

$$k_m = 59 \text{ W/m}^\circ\text{C} \quad \text{Wrought iron (Table 2)}$$

$$U_o = \frac{1}{\frac{0.0603}{0.052 \times 7500} + \frac{0.0041}{59} \times \frac{0.0603}{0.056} + \frac{1}{3200}} = \frac{1}{0.00015 + 0.000075 + 0.0003} = \frac{1}{5.25 \times 10^{-4}}$$

$$U_o = 1904.7 \text{ m}^2\text{C/W}$$

$$A_o = \frac{q}{U_o \Delta T_L} = \frac{9825 \text{ J/s}}{1904.7 \times 13.95} = 0.369 \text{ m}^2$$

$$A_o = \pi D_o L \quad 0.369 \text{ m}^2 = 3.14 \times (0.0603) L$$

$$L = 1.9 \text{ m}$$