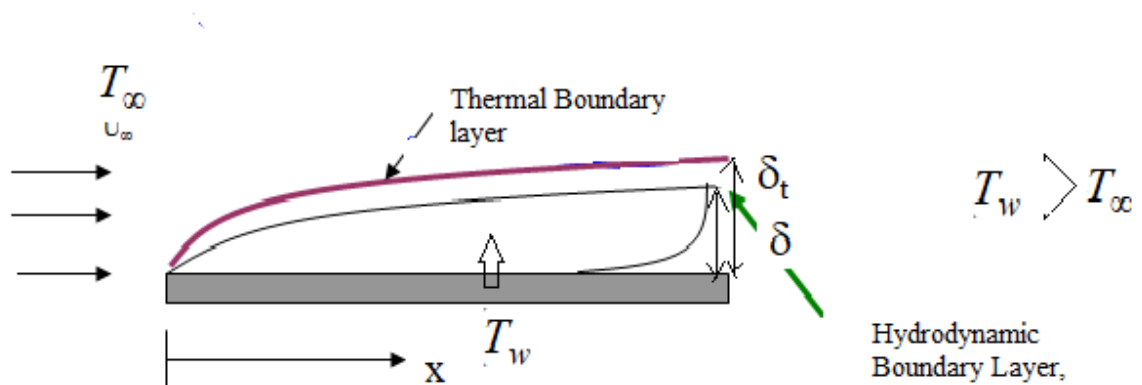


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5. Heat transfer coefficients, thermal boundary layer



$$q = -kA \left(\frac{\partial T}{\partial y} \right)_{y=0} = Ah(T_w - T_\infty)$$

Laminar flow heat transfer to flat plate

$$\bar{Nu} = 0.664 Re^{1/2} Pr^{1/3}$$

Example:

$$T_\infty = 20 \text{ }^\circ\text{C}$$

$$v = 15 \text{ m/s}$$

$$T_w = 110 \text{ }^\circ\text{C}$$

$$x = 0.5 \text{ m}$$

$$q = ?$$

$$q = h A (T_w - T_\infty)$$

$$T_f = \frac{T_w + T_\infty}{2} = \frac{110 + 20}{2} = 65 \text{ }^\circ\text{C} = 338 \text{ K}$$

Physical properties of air at 338 K (Table 5) by interpolation,

$$\begin{aligned}\rho &= 1.041 \text{ kg/m}^3 \\ C_p &= 1.0082 \text{ kJ/kg}^\circ\text{C} \\ \mu &= 2.02 \cdot 10^{-5} \text{ kg/ms} \\ k &= 0.02912 \text{ W/m}^\circ\text{C} \\ Pr &= 0.699\end{aligned}$$

$$Re = \frac{x v \rho}{\mu} = \frac{0.5 \text{ m} \cdot 15 \text{ m/s} \cdot 1.041 \text{ kg/m}^3}{2.02 \cdot 10^{-5} \text{ kg/ms}} = 386509 < 5 \cdot 10^5 \quad (\text{Laminar flow})$$

$$Nu = 0.664 \cdot Pr^{1/3} \cdot Re^{1/2}$$

$$Nu = 0.664 \cdot (0.699)^{1/3} \cdot (386509)^{1/2} = 366.36$$

$$Nu = \frac{h x}{k} = 366.36 = \frac{h \cdot 0.5 \text{ m}}{0.02912 \text{ W/m}^\circ\text{C}}$$

$$h = 21.34 \text{ W/m}^2\text{ }^\circ\text{C}$$

$$q = h A (T_w - T_\infty)$$

$$q = 21.34 \cdot 0.5^2 \cdot (110 - 20)$$

$$q = 480.15 \text{ W}$$